

EBC-Symposium 2012 „From Chiller to Filler“

# Process and plant for the **CONTINUOUS FERMENTATION** of fluids

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### + Advantages of continuous (fermentation) processes +

- Improved plant performance, due to the reduction of processing times
- Increased space-time yield
- A resulting reduction of the cost of capital
- Less space consumption due to smaller plants
- Reduced energy consumption, especially by avoiding costly energy peaks
- Reduced costs for cleaning, detergents, disinfection and amount of wastewater
- An increase in labor productivity
- Reduced personal costs
- Less losses
- Improved fermentation gas (e.g. CO<sub>2</sub>) recovery
- Less cleaning intervals
- Lower equipment costs
- Achievement of high standards of hygiene in closed systems
- Qualitative benefits
- Achievement of a constant quality of the final product



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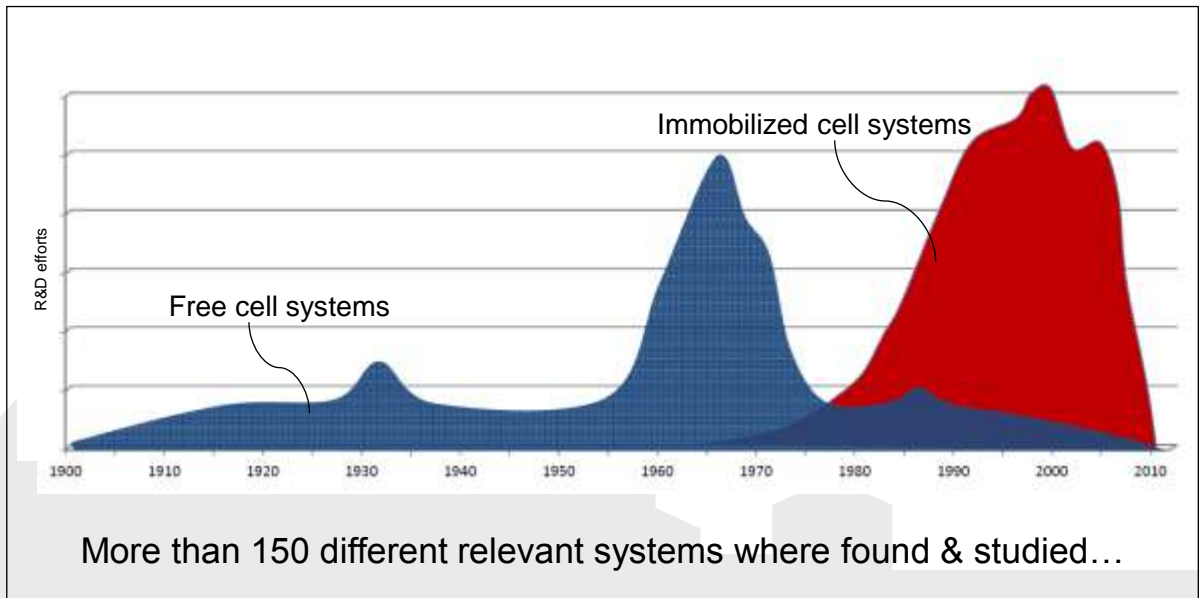
- Disadvantages of continuous (fermentation) processes -

- Lack of flexibility with respect to sales fluctuations
- Each production line can only produce one type of product
- Increased costs for proper organization of work (24-hour operation)
- Better qualified personnel is needed
- Higher expenses for the preservation of infections
- For process stability, a consistent quality of the raw materials is necessary
- Increased risk of mutations of organisms due to aging and long-term stress

**Significant changes of the product character**



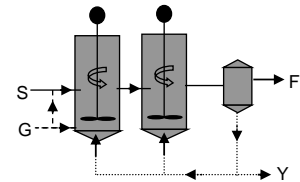
R&D effort in continuous fermentation processes





### Continuous fermentation processes in praxis

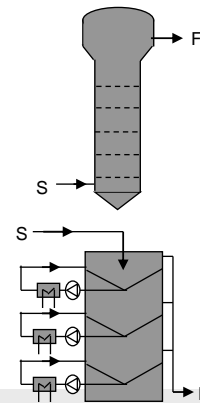
**Coutts (1959):** Dominion Breweries (New Zealand), New Zealand Breweries Ltd. (New Zealand), Canadian Breweries Ltd. (Canada), San Miguel Brewery Co. (Manila)



**Fort Worth Fermenter (1965):** Carling Brewing Company (USA)

**Bishop Process (1970):** Watney Mann (England)

**APV Tower Fermenter (1960):** Cape Hill Brewery (England), Brewery in Burton upon Trent (England), Brewery in Runcorn (England), Brewery in Warrington (England), Oranjeboom Brewery (Netherlands), Cerevecera del Norte (Spain)



**Gotha Fermentation System (1973):** Brewery Gotha (East Germany)

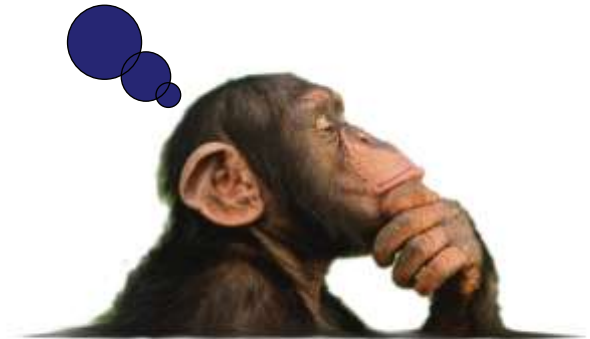


## Conclusion

- **Technology offers significant advantages, which will gain importance in the near future.**
- **In praxis only very few systems with free cells were tested (40-50 years ago!)**
- **Nearly all of them failed.**
- **Due to those failures and the potential higher efficiency the research and development has focused on systems with immobilized cell reactors.**

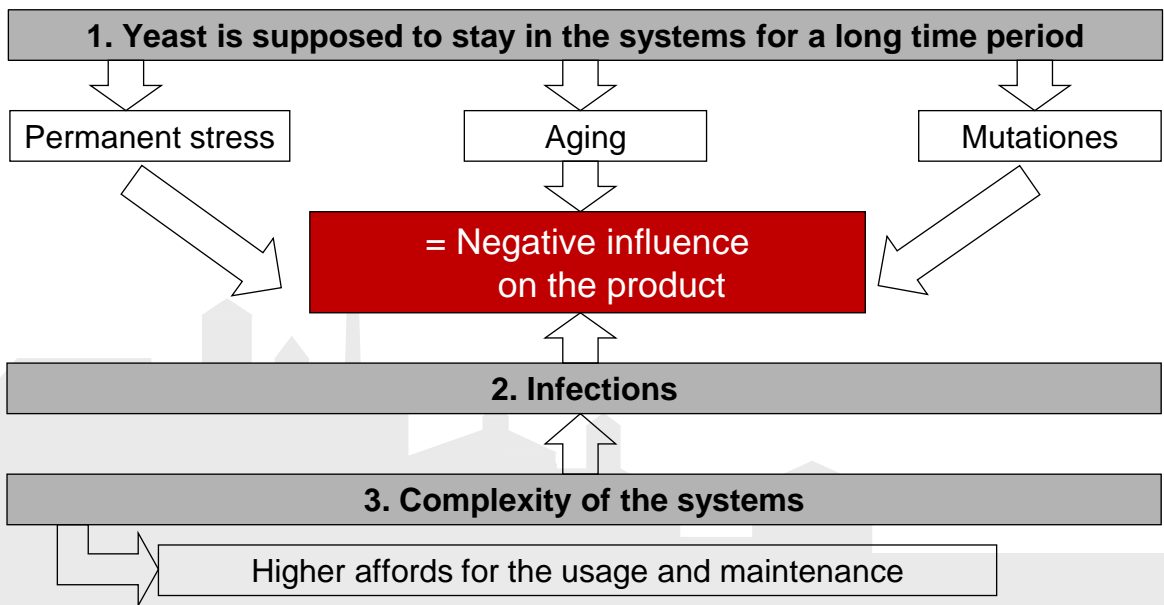


- Does further research in this field make sense?
- Why did systems fail in the past?
- Which systems should be preferred; Immobilized or Free-Cell Systems?





Main reasons for the failure of existing systems





**Demands**

**1. Yeast should be treated nearly identically to classical batch process**

**2. System has to be safe against infections**

**3. Simple construction and usage**

4. Integable into existing plant

5. Multifunctionality

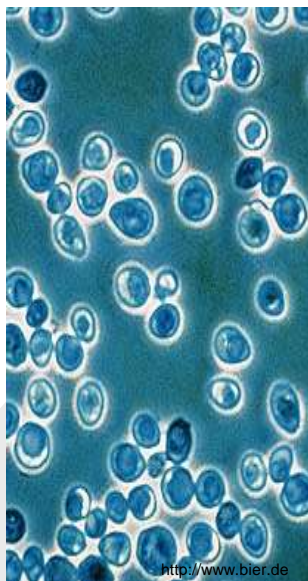
6. Usage of existing equipment if possible

**Economic and ecological advantages**  
**High constant product quality**





Key to success: Properties of the yeasts



<http://www.bier.de>

**Yeasts determine the product character!**

Intentionally adapted to batch process since centuries

Significant gain of knowledge within the past 40-50 years!

**Influence:**

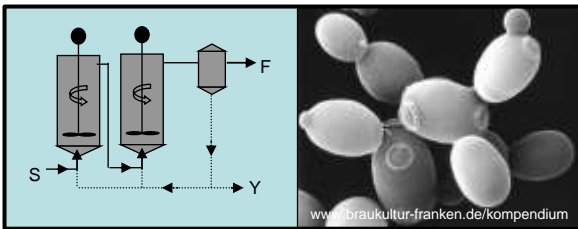
- Temperature
- Pressure
- Substrate properties
- Aeration
- Cell amount
- Age



<http://truthfall.com>



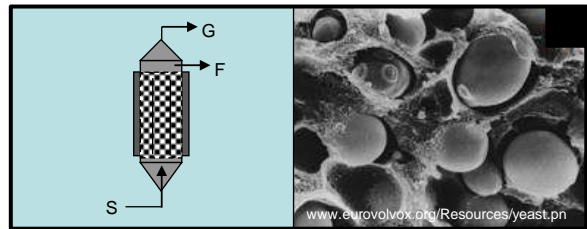
Free cell systems



- + Yeast cycles can be reproduced
- + Aged yeast can be discharged
- + Lower risk of permanent infections

- Larger reactors
- More produced biomass
- Rather complicated systems
- = **Lower Efficiency?!?**

Immobilized cell systems

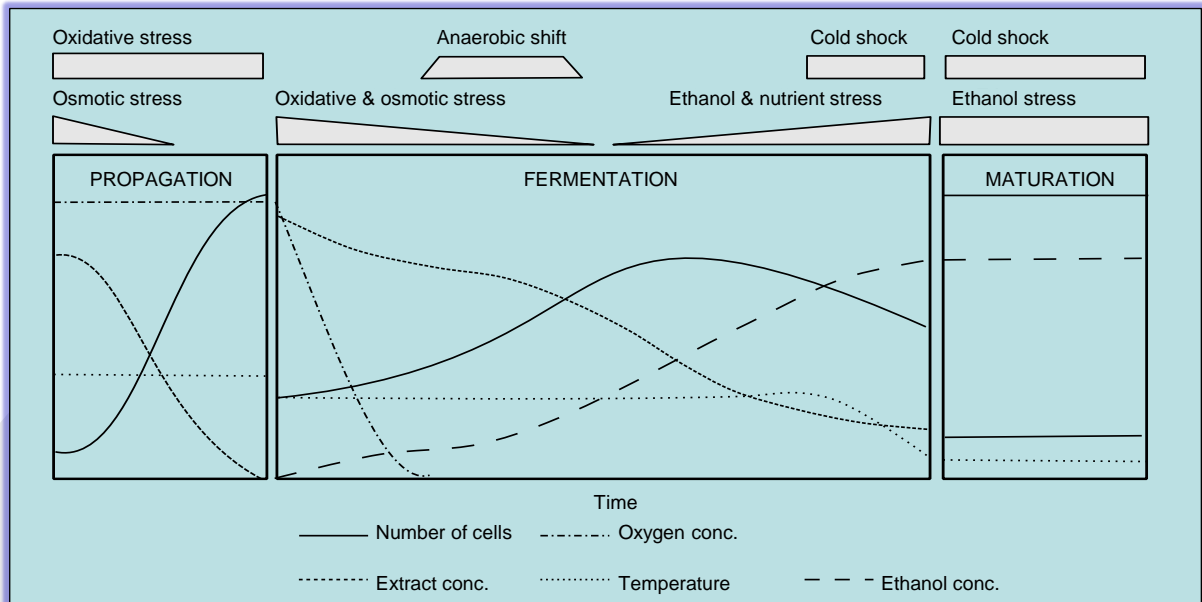


- + Small reactors
- + Less produced biomass
- + Uncomplicated systems
- = **Higher Efficiency?!?**

- Long term stress for yeasts
- Yeast ages in system
- Higher risk of yeast mutations
- Higher risk of permanent infection



Stress situations for yeasts in the brewery

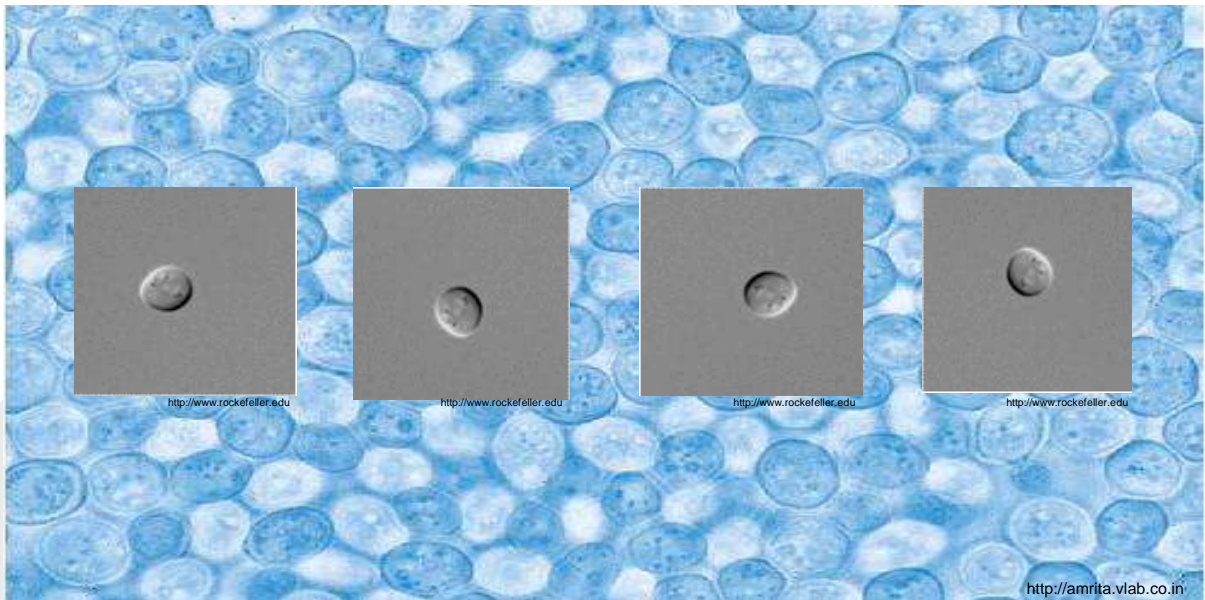


Brewers: Traditional & hard to convince...



[www.langersamstag.ch/media/bierbrauer-susch.jpg](http://www.langersamstag.ch/media/bierbrauer-susch.jpg)

Systemes with free cells!!!





### Patent- & literature research: Free cell systems



#### Conclusion

Many systems are very complex

Often many mechanical parts are being used

Difficult clean ability → higher risk of infections

Commissioning times are often long

Nearly no system focuses on yeast demands

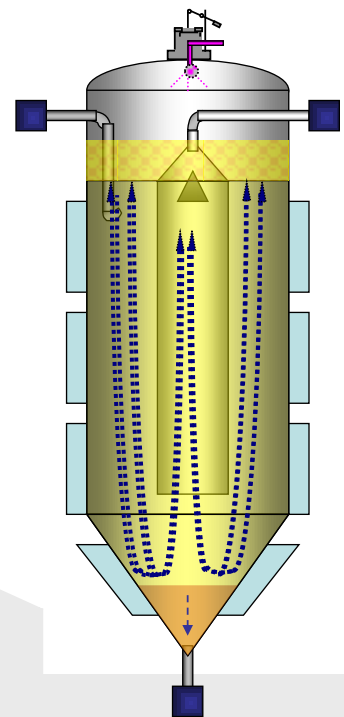
Yeasts are supposed to stay in systems for long time periods

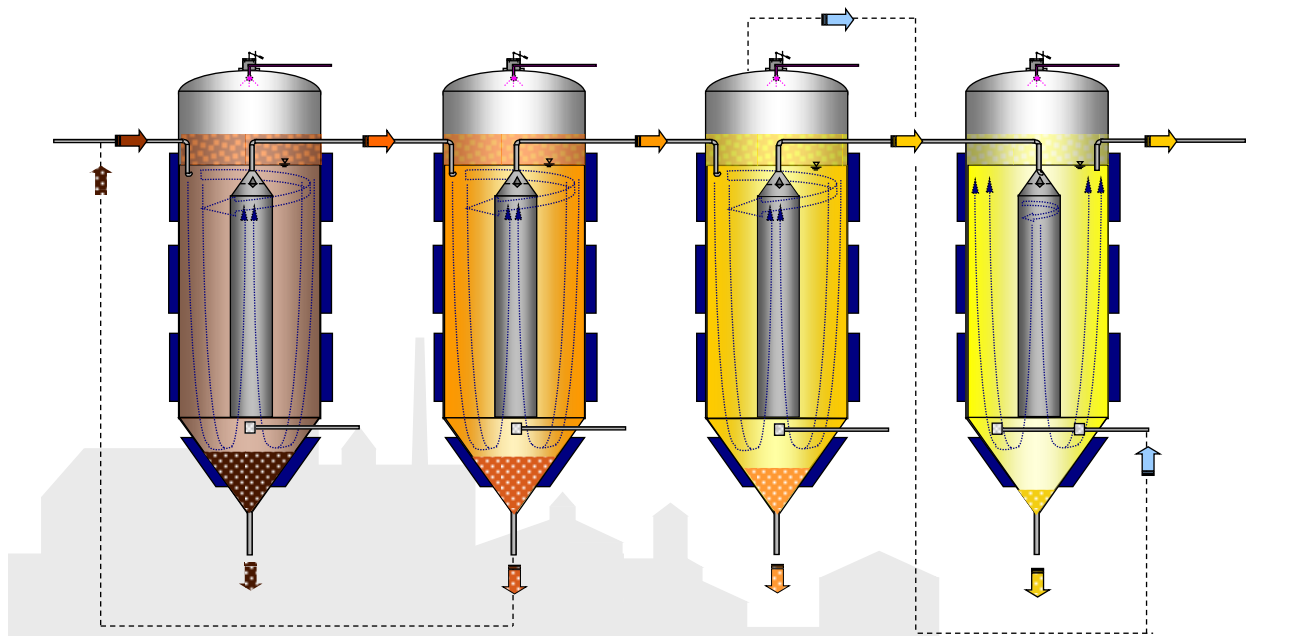
Often no possibility to remove yeasts and particles regularly



### Conception: Free cell system

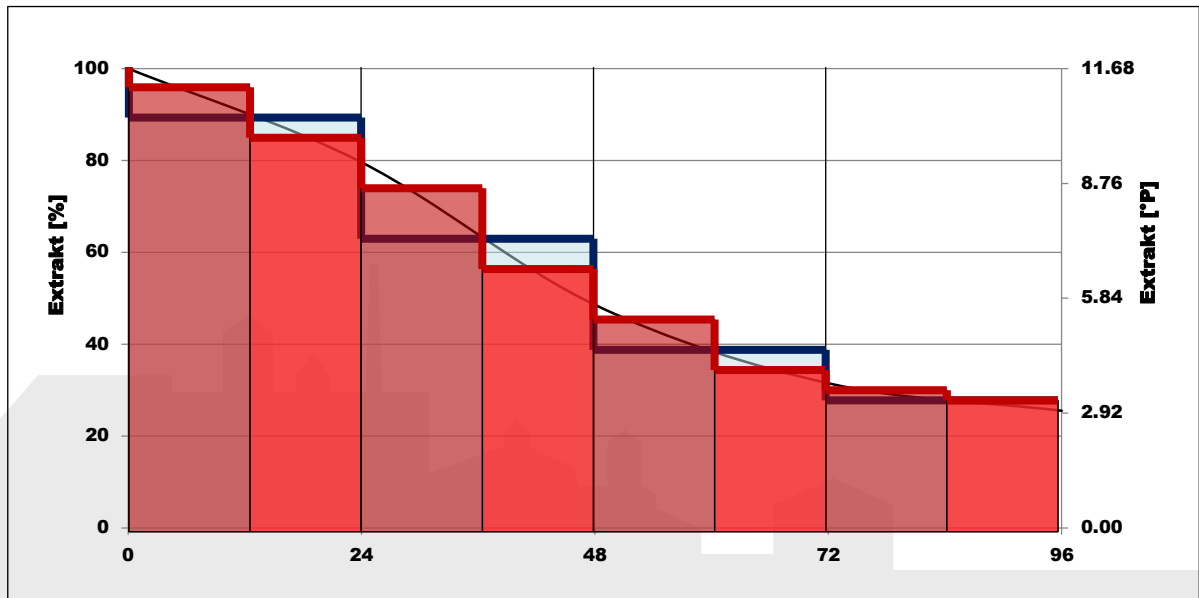
- Usage of state of art equipment!
- Simple installation of a central conduction pipe through which the fermentate can be charged or discharged
- Other installations for intake/outtake in the top part of the tank are foreseen
- Further equipment like a cooling system for the conduction pipe may be integrated
- Particles and yeasts can be discharged at the tank bottom
- The system is operated continuously or at least semi-continuously





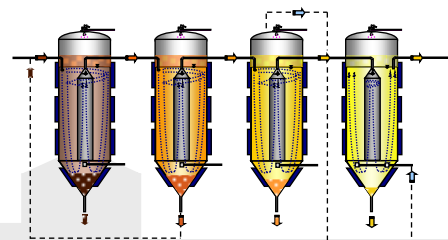
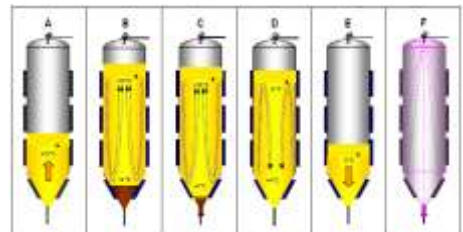


Fermentation progress & resulting yeast stress



## Advantages of this concept

- The yeast cycles, as they exist in classical batch fermentations can be simulated
- Particles (e.g. trub, yeasts) as well as gases can be discharged and added to the process variable
- Pressure and temperature gradients can be adjusted precisely.
- Existing plants may partly be used by modification
- The function, commissioning, as well as the cleaning and maintenance are fairly easy



--? Economic advantages ?--



### Simplified calculation

In a classical batch fermentation the filling time and the discharge times should each not be longer than 10% (referring to the fermentation)  
(Example: 5 days main fermentation = 120h: Filling/discharge time<sub>max</sub> = 12h each)

**Longer filling and discharge cycles would lead to the following disadvantages**  
**(Independent of batch size!)**

- Due to the longer supply of amino acids more Diacetyl will be produced
  - The oxygen supply might lead to oxidations
  - The yeast cycles may be disrupted
  - The content can not be cooled fast enough



Simplified calculation

Classical Batch Fermentation

Filling	Fermentation	Discharge	CIP	Occupation time	Necessary tanks	Tanks/day	Tank size
12 h	5 days	12 h	4 h	148,0 h	14 tanks	2	50% daily production
9,6 h	4 days	9,6 h	3,2 h	118,4 h	14 tanks	2,5	40% daily production
<b>7,2 h</b>	<b>3 days</b>	<b>7,2 h</b>	<b>2,4 h</b>	<b>88,8 h</b>	<b>14 tanks</b>	<b>3,3</b>	<b>30% daily production</b>
4,8 h	2 days	4,8 h	1,6 h	59,2 h	14 tanks	5	20% daily production
2,4 h	1 day	2,4 h	0,8 h	29,6 h	14 tanks	10	10% daily production

Continuous Fermentation

Filling	Fermentation	Discharge	CIP	Occupation time	Necessary tanks	Tanks/day	Tank size
	5 days			120 h	5+1 Tanks		100% daily production
	4 days			96 h	4+1 Tanks		100% daily production
	<b>3 days</b>			<b>72 h</b>	<b>3 +1 Tanks</b>		<b>100% daily production</b>
	2 days			48 h	3+1 Tanks		66% daily production
	1 day			24 h	3+1 Tanks		33% daily production



### Costs of a modern tank cleaning with fresh substances

Detergent	Consumption	Price/Unit [Euro]	Costs[Euro]
Water[m <sup>3</sup> ]	5,6	3,83	21,47
Caustic [l]	37	0,07	3,07
Acid [l]	6,9	0,81	5,58
Desinfection [l]	1,3	1,76	2,29
<b>Total costs [Euro]</b>			<b>32,41</b>

Heating energy	Consumption	Price/Unit [Cent]	Costs [Euro]
1. Step 45°C [kWh]	85,2	1,55	1,32
2. Step 65°C [kWh]	221,6	1,55	3,42
<b>Total costs [Euro]</b>			<b>4,74</b>

**Approx. Costs for the cleaning of one tank**

**37,15 Euro**



Simplified calculation

Classical Batch Fermentation

Fermentation time	Tank size	Costs per tank cleaning	Tanks/day	CIP costs/day	300 days production/a
5 days	100%	37,15 Euro	2	74,3 Euro	22.290 Euro/a
4 days	80%	29,72 Euro	2,5	74,3 Euro	22.290 Euro/a
<b>3 days</b>	<b>60%</b>	<b>22,29 Euro</b>	<b>3,3</b>	<b>74,3 Euro</b>	<b>22.290 Euro/a</b>
2 days	40%	14,86 Euro	5	74,3 Euro	22.290 Euro/a
1 day	20%	7,43 Euro	10	74,3 Euro	22.290 Euro/a

Continuous Fermentation

Fermentation time	Tank size	Costs per tank cleaning	Tanks/day	CIP costs/day	365 days production/a
5 days	100%	37,15 Euro	0,16	6,19 Euro	2.229 Euro/a
4 days	100%	37,15 Euro	0,13	4,95 Euro	1.783 Euro/a
<b>3 days</b>	<b>100%</b>	<b>37,15 Euro</b>	<b>0,1</b>	<b>3,72 Euro</b>	<b>1.337 Euro/a</b>
2 days	66%	24,52 Euro	0,1	2,45 Euro	883 Euro/a
1 day	33%	12,25 Euro	0,1	1,23 Euro	441 Euro/a



## Conclusion

### **Plant concept with focus on simplicity with focus on brewery yeast demands**

#### **Technological advantages**

- **Low stress for yeasts**
- **Fractionization of particles, gas and organisms possible**
- **Yeast can live through the same cycles like in batch process**

#### **Economical and ecological advantages**

- **Less tanks = less needed space, lower investment costs, less equipment-, control-, and cleaning efforts necessary**
- **Less waste / consumption (beer, water, gas, CIP, yeast, energy, cooling...)**
- **Constant product quality**



But: not everything can be calculated or predicted...

**Open questiones:**

For which drinks is such a technology suitable?

Can realistic conditions be achieved in small scale?

How should experiments be conducted in order to allow scale up?

What are the ideal parameters for a fast fermentation?

How does standard yeast react?

How can the physiological condition of the yeast be measured simple?

Can a small scale plant be built and be run under similar conditions?

How does such a product taste like?

How stable can such a plant be run?

How does the system react to infections?

How can the performance be optimized?



### 1. Investigation in order to evaluate the process suitability

In total **278 !!!**  
different fermented beverages were investigated

*152 Drinks were made out of cereals or pseudo-cereals*

*56 Drinks were milk-based*

*17 Drinks were fruit-based*

*53 beverages were made out of different ingredients*

Name of beverage	Raw material & additives	Origin	Fermentation time	Fermentation temp.	MO	Literature



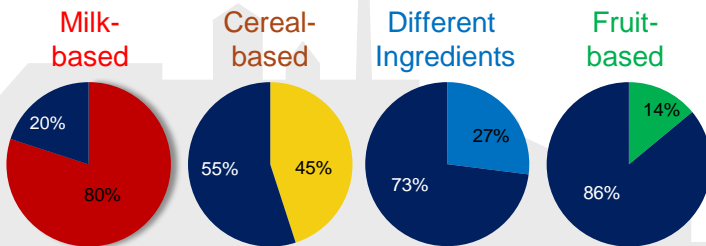
Name Getränk	Rohstoff u. Zusätze	Fermentation			MO	Quelle
		Land	Dauer	Temperatur		
<b>Bananen-Bier</b>						
Isongo	Bananensaft, gerösteter Sorghum	Burundi	48-96 h	14-25 °C	Sac1	30, 105, 18 (S.89)
Lubisi	Bananen, Sorghum	Uganda	18-24 h	14-25 °C	Sac1	106, 105, 18 (S.89)
Mbege	Bananen, Fingerhirse	Tansania	96-120 h	14-25 °C	Sac1	107, 108, 105, 18 (S.89)
Mwenge	Bananen, Sorghum	Uganda	18-24 h	14-25 °C	Sac1	106, 105, 18 (S.89)
Urwarwa/Urwegwa	verdünnter Bananensaft, gerösteter Sorghum	Burundi, Rwanda	48-96 h	14-25 °C	Sac1	30, 106, 105, 18 (S.89)
Urwaga	Bananen, Sorghum, Hirse o. Mais	Kenia	18-24 h	14-25 °C	Sac1	106, 105, 18 (S.89)
<b>Bananenwein</b>						
Malkia	Bananen	Tansania	2-8 Wochen	k. A.	k. A.	108, 109
Meru	Bananen	Tansania	2-8 Wochen	k. A.	k. A.	108, 109
Raha	Bananen	Tansania	2-8 Wochen	k. A.	k. A.	108, 109



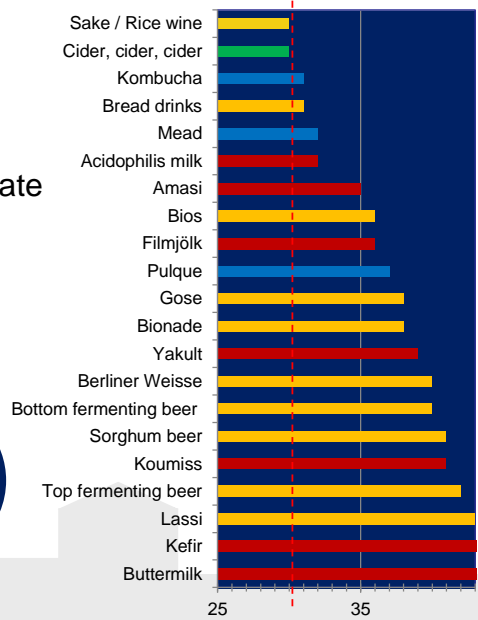
Assessment of 49 types of beverages

1. Raw materials
2. Sales volume
3. Production period
4. Fermentation time
5. Production site
6. Sales area / Market

$\geq 40$  P = good  
 $30-39$  P = suitable  
 $20-29$  P = not appropriate  
 $< 20$  P = not suitable

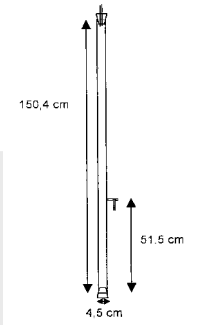
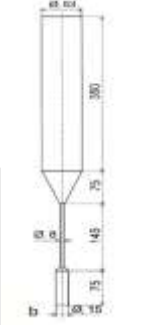
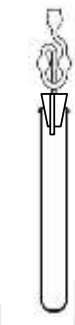



■ = not suitable



2. Can small scale fermentations reflect realistic situations?

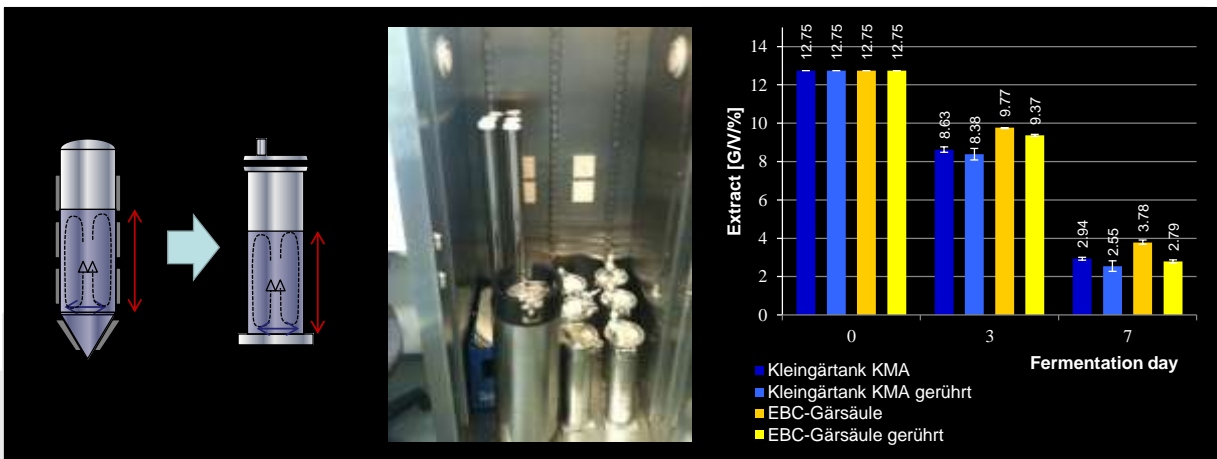
3. How should they be done in order to allow a scale up?

EBC fermenter	Lietz fermenter	Laboratory fermenter	Weinfurter fermenter
 A schematic diagram of an EBC fermenter. It is a vertical cylindrical vessel with a diameter of 4.5 cm and a total height of 150.4 cm. A smaller section at the bottom has a height of 51.5 cm. The diagram shows the internal structure and various ports.	 A schematic diagram of a Lietz fermenter. It is a vertical cylindrical vessel with a diameter of 100 mm and a total height of 300 mm. The diagram shows a conical bottom section and various internal components.	 A schematic diagram of a laboratory fermenter. It is a vertical cylindrical vessel with a diameter of 100 mm and a total height of 140 mm. The diagram shows a central stirrer shaft and a top-mounted motor.	 A schematic diagram of a Weinfurter fermenter. It is a vertical cylindrical vessel with a diameter of 100 mm and a total height of 140 mm. The diagram shows a complex internal structure with multiple stirrer blades and a top-mounted motor.



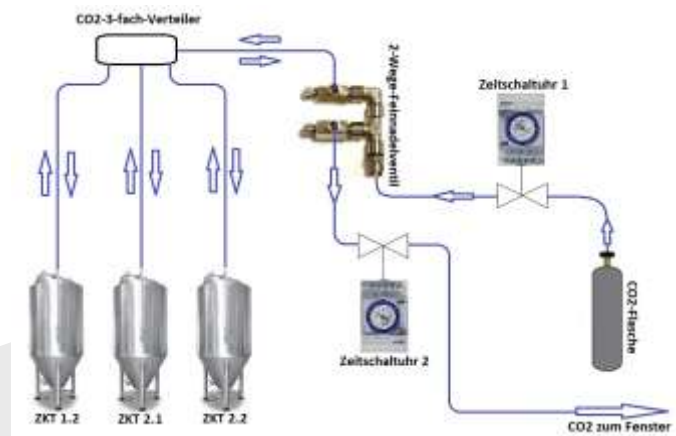
2. Can small scale fermentations reflect realistic situations?

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2. Can small scale fermentations reflect realistic situations?

3. How should they be done in order to allow a scale up?

Tests in order to check different substrates for their suitability

Richtwerte	Normwert	W	E1	E2	E3	E4	E5	E6	G1	P1	P2
FAN [mg/l]	200 - 240	208	153,8	101,7	42,9	89,1	23,2	49,2	170,5	133,2	89,8
Summe AS [mg/l]	1600-2000	1694	1249	826,3	348,5	723,5	188,7	399,4	1384,7	1082,3	729,2
pH- Wert	5,2	5,2	5,07	5,28	5,53	5,71	4,77	5,5	5,33	5,26	5,75
Ges. Lösl. N [mg/l]	900 - 1100	1056	1303	1071	450	721	875	544	980	1302	651
noch koagl. N [mg/l]	< 25	21	34	43	15	57	36	19	9	53	64
Scheinbarer Extrakt [G/V%]	12	12,18	11,98	12,08	12,1	12,26	12,17	12,18	12,53	12,58	12,52
Farbe	5 - 15	12	13	15	19	25	77,5	19	55	31,3	11,25
TBZ	< 45	29,5	119,5	116,8	283	66,6	1239	94,9	82,7	280	47,5
Fructose [g/l]	1-2	1,52	1,9	1,68	0,71	0,1	0,51	0,1	0,5	0,49	0,02
Glucose [g/l]	10-12	10,86	13,09	12,41	8,31	2	10	2	3,51	3,03	1,5
Saccharose [g/l]	2-4	3,01	3,08	2,55	0,88	1,5	0,25	1	2,5	0,41	1,7
Maltose [g/l]	56-80	70,61	61,04	66,19	57,45	4,92	12,3	18,03	18,87	16,4	5,73
Maltotriose [g/l]	14-17	15	13,75	18,58	22,89	4,02	2,5	6	7,51	6	5,01



#### 4. & 5. Reactions to different situations

##### Fermentations under the variations of

- Cell amount (4 different)
- Aeration (aerated/not aerated)
- Temperature (3 different)
- Pressure (3 different)

##### Additional tests

- Alkohol stress
  - Pressure stress
  - High-Gravity-Stress
  - Pressure variations
- 3 usages,  
different  
steams

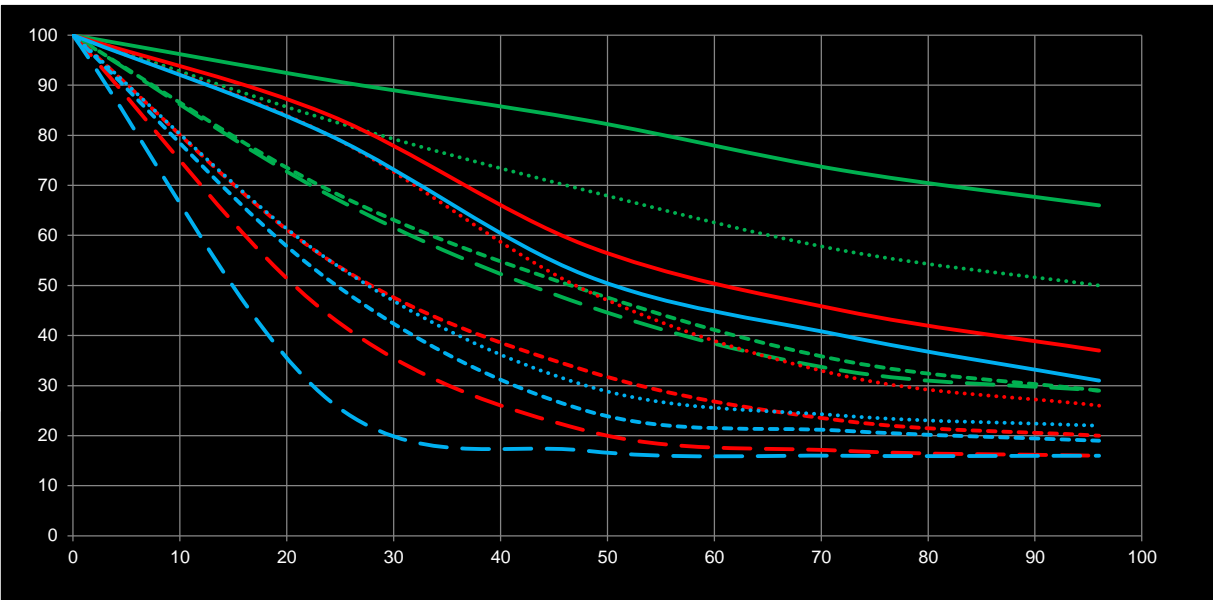
Tests for over one year!!!

##### Analyses

Extrakt  
pH-Value  
Alkohol  
FAN (alleAA!)  
VDK  
Biomass/Cell count  
GCs



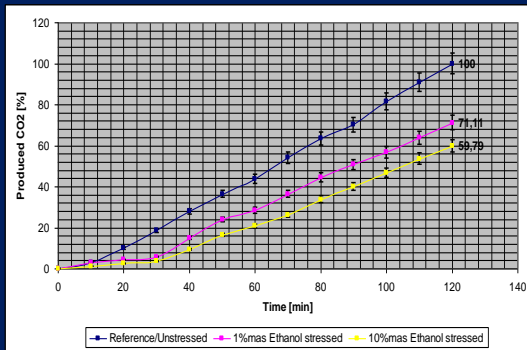
4.& 5. Reactions to different situations



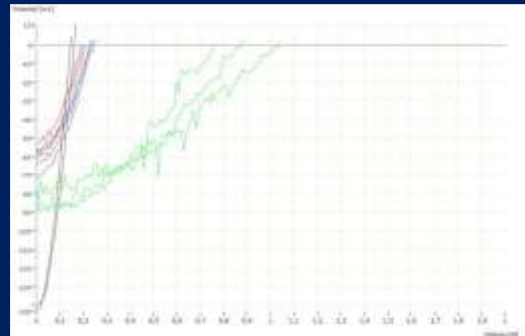


6. Simple method in order to determine the yeast vitality

Via CO<sub>2</sub>-built up



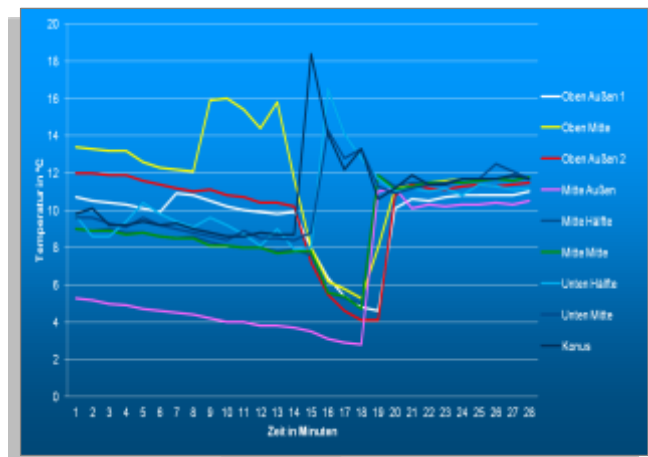
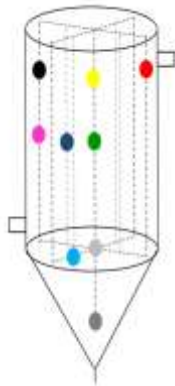
Via particle size analysis



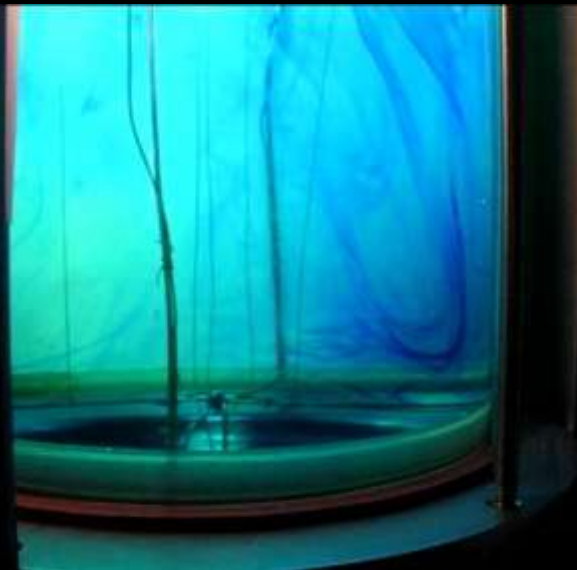
Technology: Possibilities in small scale



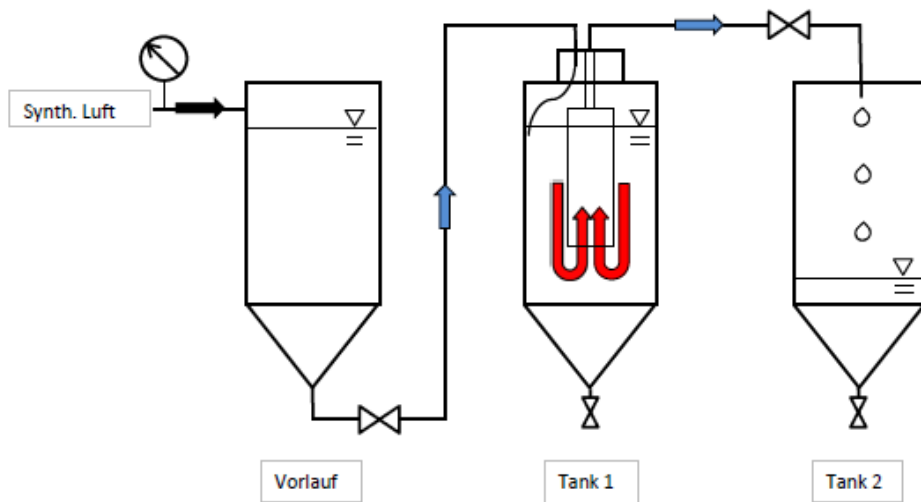
Technology: Possibilities in small scale



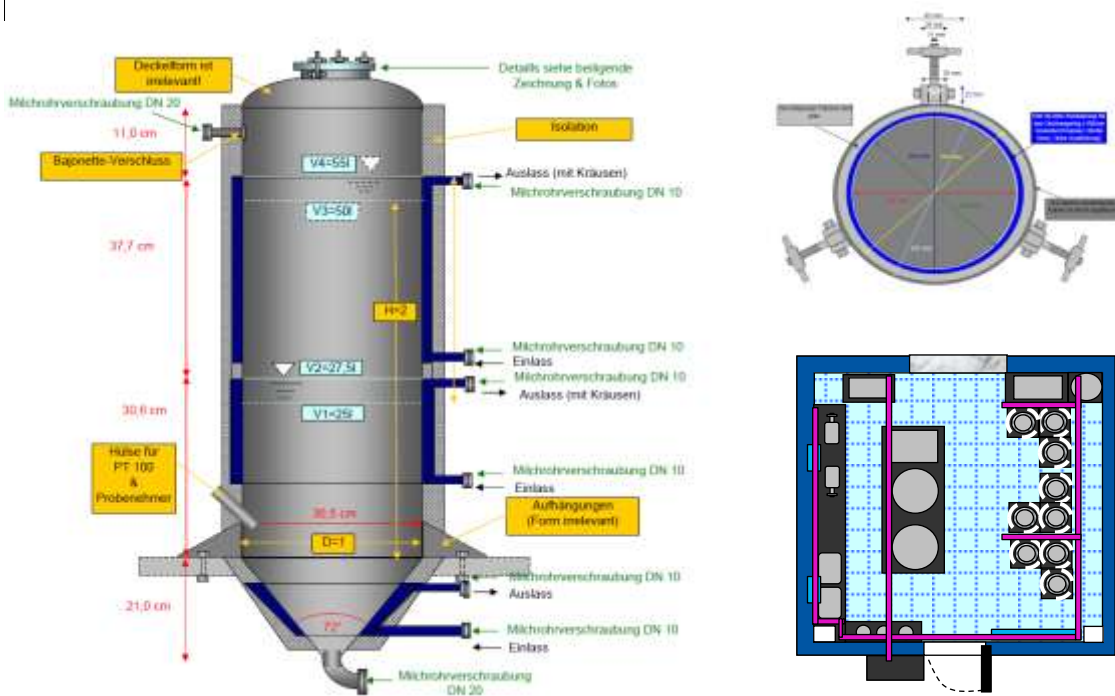
Technology: Possibilities in small scale



Technology: Possibilities in small scale









R & D

## Continuous Fermentation



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für Brau- und Lebensmittelqualität



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## Experiments & Results

### **1-Tank Process (6 days)**

- No bigger process problems
- Currency tests successful
- Only small changes/simplifications necessary

### **3-Tank Process (33 days)**

- No process problems
- Extract, Alcohol, pH-Value relatively constant
- Taste: constant good
- Contamination with wort bacteria: No long term problem!

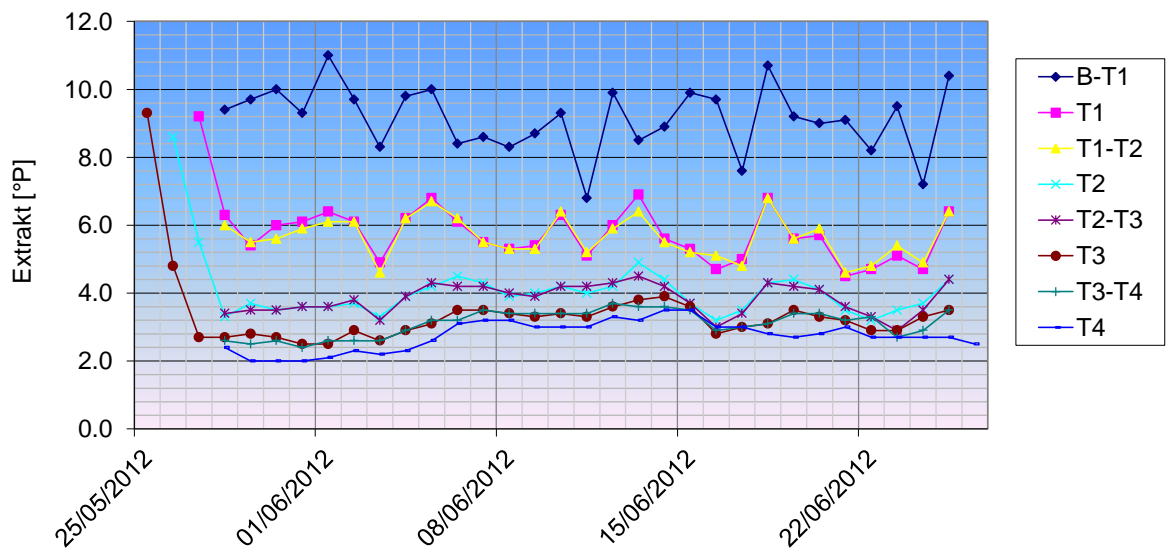
10 filling, discharging and CIP processes per tank less!!!  
= totally 30-40x less!!!

### **4-Tank Process (35 days)**

- No process problems
- Extract, Alcohol, pH-Value relatively constant
- Taste: constant good
- Contamination with different bacteria: No long term problem!

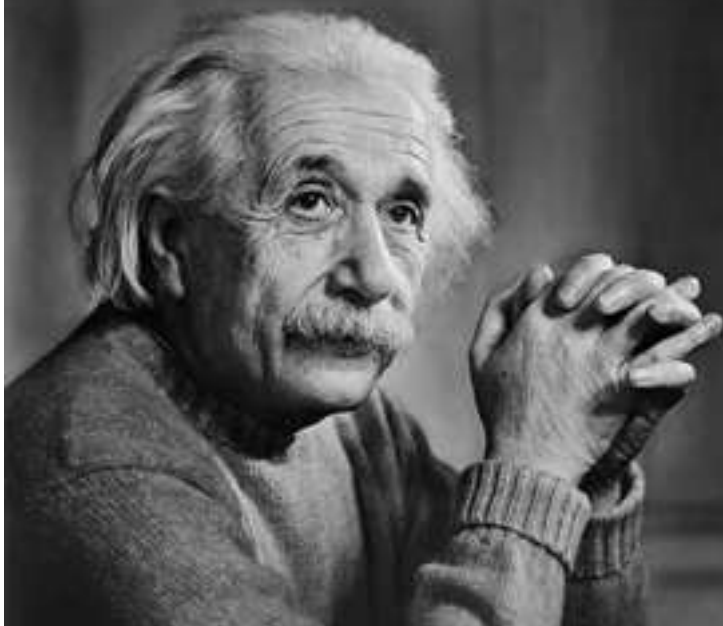


Results



If you can't explain it **simply**, you don't understand it well enough.

– Albert Einstein





**Thank you for your attention!**

**Dipl.- Ing. Konrad Müller-Auffermann**

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Future trends in the beverage industry

Energy efficiency

Sustainability

Transparency

Individuality

Funktionalität

Economy // Price

Continuous fermentation

